

Me899 lecture 06 - small-scale fluid flows

As scale decreases, surface/volume increases so friction increases

→ slip counteracts this

Knudsen number = quantifies importance of slip

$$Kn = \frac{\lambda}{L_0} \quad \begin{array}{l} \lambda \text{ --- mean free path} \\ L_0 \text{ --- length scale} \end{array} \quad \text{gases}$$

$$Kn = \frac{b}{L_0} \quad \begin{array}{l} b \text{ --- slip length} \end{array} \quad \text{liquids}$$

e.g., $L_0 = \text{pipe diameter}$

start from the ideal gas law,

$$p = n k_B T$$

k_B Boltzmann's constant, $1.38 \times 10^{-23} \text{ J/K}$
 n # density = $2.7 \times 10^{25} / \text{m}^3$

$$\text{mean molecular spacing, } d \propto n^{-1/3} \approx 3 \times 10^{-9} \text{ m} = 3 \text{ nm}$$

$$d = \text{hard sphere diameter} \approx 10^{-10} \text{ m}$$

so we define a "dilute gas" $\Rightarrow d/d \gg 1$

\Rightarrow mostly atom-atom collisions

rather than multi-atom collisions

gas mean free path

$$\lambda = \frac{1}{\pi d^2 n \sqrt{2}} = \frac{kT}{\pi P d^2 \sqrt{2}}, \quad \text{substituting the ideal gas law}$$

\downarrow \leftarrow $f(\text{pressure})$
 hard sphere diameter

flow regimes:

$$Kn < 0.01 = \text{continuum (no slip)}$$

$$0.01 < Kn < 0.1 = \text{slip}$$

$$0.1 < Kn < 10 = \text{transition}$$

$$Kn > 10 = \text{"free molecule"} \sim \text{macroscopic property meanings break down}$$

\Rightarrow direct simulations of Boltzmann equation

example of λ : air @ 1 atm, 300 K, $\lambda = 65 \text{ nm}$

0.001 atm, 300 K, $\lambda = 65 \mu\text{m}!$

1 atm, 1200 K, $\lambda = 2.6 \mu\text{m}$



microchannel $< 250 \mu\text{m}$
is in slip regime

Navier-Stokes eqns for unsteady incompressible flow

$$\frac{d\vec{v}}{dt} = -\frac{\nabla P}{\rho} + \nu^2 \nabla^2 \vec{v} + f, \quad \nu = \frac{\mu}{\rho}$$

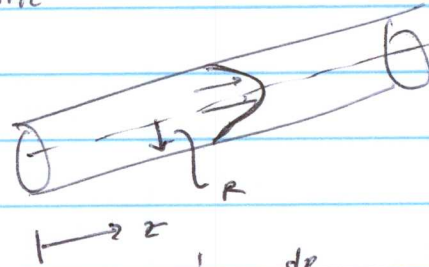
$$\nabla \cdot \vec{v} = 0$$

⇒ let's quantify the effect of slip on friction in a small pipe

flow is 1-dimensional, θ -symmetric

reduced N/S eqn.

$$+\frac{1}{\mu} \frac{dp}{dz} = \frac{1}{r} \frac{d}{dr} \left(r \frac{dv(r)}{dr} \right)$$



$$\frac{dp}{dz} = \text{constant}$$

steady, fully-developed flow

solve for velocity profile in the pipe, $v(r)$

tangential velocity is neglected here

$$\iint + \frac{r}{\mu} \frac{dp}{dz} = \iint \frac{d}{dr} \left(r \frac{dv(r)}{dr} \right)$$

$$\int \left(\frac{+r^2 \frac{dp}{dz} + c}{r} \right) = \int \frac{dv(r)}{dr}$$

$$\frac{+r^2}{4\mu} \frac{dp}{dz} + c \ln r = v(r) \quad \Rightarrow v(0) \text{ is finite so } c = 0$$

$$\text{for no-slip, } v(R) = 0, \text{ so } D = -\frac{R^2}{4\mu} \frac{dp}{dz}$$

